

Measuring N₂O Emissions at Zaandam-Oost and Apeldoorn WWTPs

This study was carried out at two wastewater treatment plants in the Netherlands. They are typical sites designed for full biological nitrogen removal, with nitrification and denitrification.

The Apeldoorn WWTP serves approx. 350,000 PE. Mainstream biological treatment via denitrification and nitrification takes place in 2 parallel modified University of Cape Town (mUCT) reactors with an anaerobic selector as well as anoxic and bottom aerated aerobic zones. The reactor under investigation (excl. anaerobic zones) is 18,800 m³.

The Zaandam-Oost WWTP serves approx. 200,000 PE. The biological treatment consists of an initial mUCT reactor with short retention time and a carousel reactor consisting of 4 serial aerated channels with bottom aeration. The latter raceway reactor with a volume of 6,800 m³ is being investigated here.

measure
to kN₂O_w

Case Study: Positioning of N₂O sensors in typical biological wastewater treatment processes

Two liquid phase N₂O sensors accurately represent process dynamics and emissions in most common raceway and recirculation reactors.

Where to Measure Nitrous Oxide (N₂O) Emissions?

This study showed that recirculating reactor types have a homogenous distribution of dissolved N₂O in the aerated zone. A single sensor is therefore representative to determine emissions from the whole zone. In the anoxic zone, the potential for loads carried over to the aeration must be monitored at the end of this zone. Deammonification reactors should be considered separately and equipped with specific sensors heads due to their high emission potential.



How to Measure N₂O in a Recirculation Reactor

The mUCT reactor investigated here is one of the most widely used reactor types in the Netherlands and many other parts of the world. This recirculation reactor is characterized by two separate ring-shaped treatment zones: An inner anoxic zone and the outer aerobic ring.

Primary Settled wastewater enters the anaerobic selector in the middle, then it flows to the inner anoxic ring. Afterwards it enters the outer ring, which is equipped with 2 separately controlled aeration fields. The flow pattern also includes a return of flow from anoxic to the selector as well as from aerobic to anoxic (Fig 1A).

As N₂O can be a byproduct of both nitrification and denitrification, it is paramount to measure in both these zones to gain a full understanding of the tank's N₂O production patterns. While most of the emissions take place in the aerated zone by air stripping, diffusion from the anoxic zone can also play a role (emission calculation described in references¹).

The carrousel reactor in this study is representative of many recirculation reactors with a raceway geometry. It consists of 4 sequential channels with aeration controlled separately by NH_4 setpoints.

Dissolved N_2O concentrations were measured with Unisense Environment N_2O Wastewater Sensors, which remained in each position between 15 and 111 days. See Figure 1A and 2A for the flow pattern and measurement locations in both reactors.

The goal of this study was to investigate spatial concentration differences along the flow direction and determine the most representative positions for long term monitoring with the purpose of emission determination and process understanding.

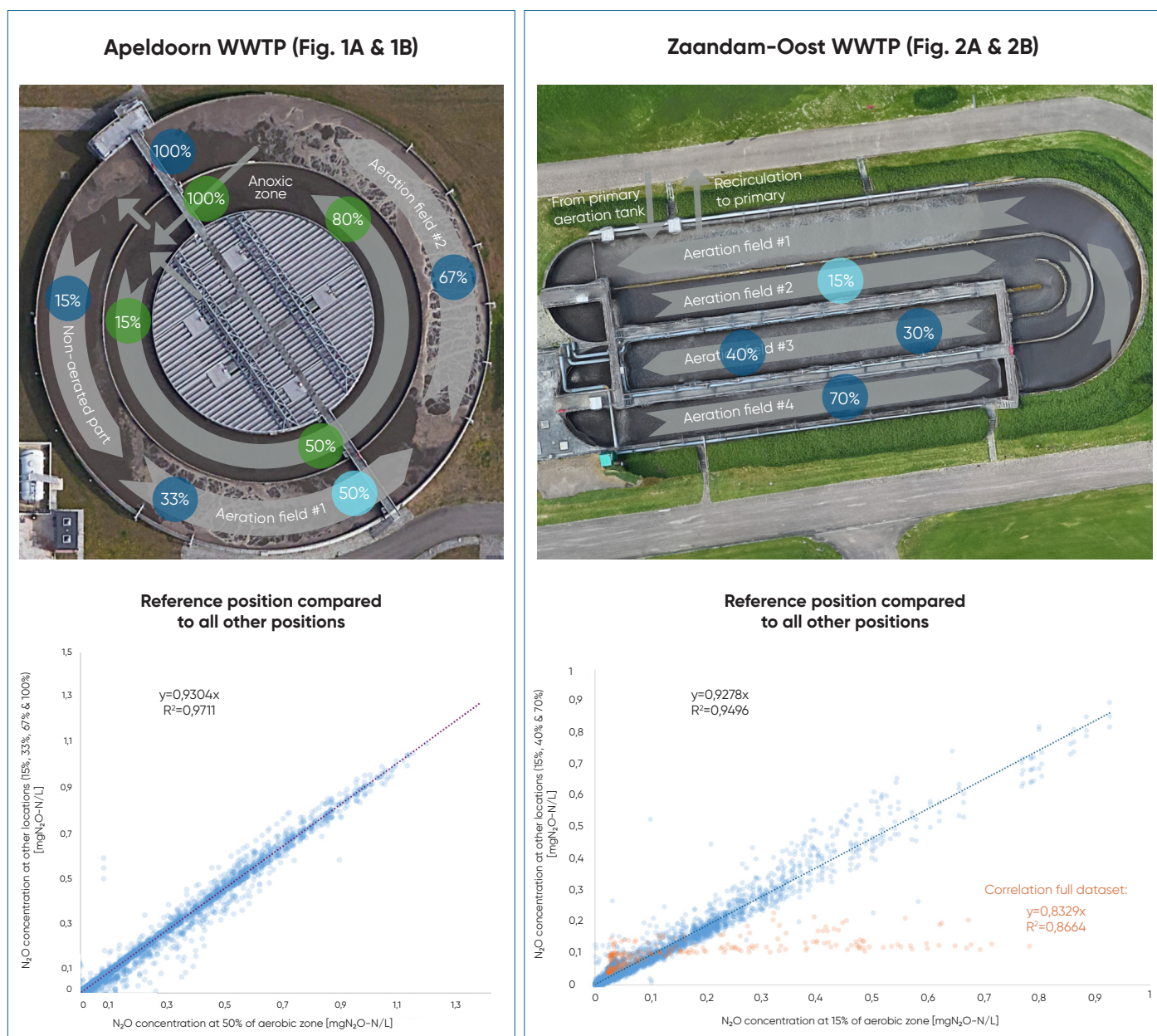


Fig 1A & 2A: Measurement locations and comparison of N_2O concentrations. Flow direction is shown by arrows, measurement position by colored dots. % gives the position within the whole length of the respective zone. Blue: aerobic zone. Light blue: reference sensor. Green: anoxic zone.

Fig 1B & 2B: Hourly average N_2O concentrations measured in the aerobic zones of the reactors. Comparison between the reference sensor position with all other locations is shown. Each position was monitored for 15–111 days. Linear correlation is shown as dotted line and formula. Orange cluster in 2B represents a 10-day event excluded from the correlation (see discussion).

Results and discussion

The measurement campaign showed that in the aerated zones, despite a large range of measured concentrations and different oxygen levels, there was no significant difference between the positions tested. This pattern was observed over a total period of 111 days and is illustrated in figure 1B and 2B. These show the direct comparison of the N_2O value at a single location (50% and 30% respectively) with all other positions in the same reactor. The linearity and correlations are very strong, with a slope as well as R^2 value close to 1 and the intercept close to zero, indicating the near equality of the concentration values measured at the different locations. A value of 1 in R^2 value would be a perfect match between values.

The orange-marked cluster in figure 2B are elevated values that were registered during a 10-day period at the position 15%, close to the influent of the reactor. Operators were not able to identify a specific technical cause for this. However, just before the period, there was a short-term change in influent configuration, resulting in unsettled sewage entering close to position 70%. It can be speculated that this upset of the process has caused the later local increase in N_2O . Due to the delimited nature of the event, the data cluster was removed from the correlation analysis. The data with the cluster included is shown in figure 2B.

In the anoxic zone a different pattern was observed, as could be expected. Depending on process conditions, this zone can be either a source or a sink of N_2O . The different positions along the zone showed marked differences in concentration. Differences also varied over time representing changes between net production or net consumption of N_2O over the whole zone.

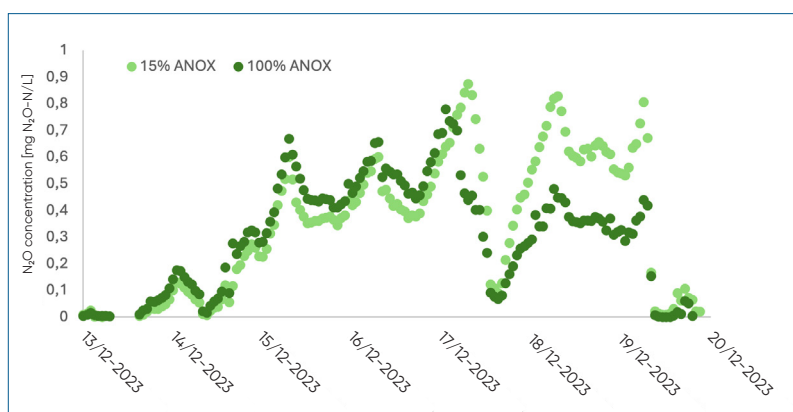


Fig. 3: Hourly average N_2O concentrations in two locations of the anoxic zone in the mUCT reactor at Apeldoorn WWTP. 15% and 100% were chosen as representative locations for illustration purposes.

Figure 3 shows a comparison of two measurement locations over the course of one week. The data is taken from 15% and 100% of the whole anoxic zone length, representing the beginning and the end of the zone.

During the first days, both locations had similar low concentrations. After that there was a period of slightly higher concentrations at 100%, speaking for net production throughout the zone. From 17.12. onward, higher concentrations in the beginning of the zone were measured, indicating a net consumption of N_2O . After this, values in both locations were similar again. These trends show the dynamic nature of bacterial processes in the anoxic zone, which can act as both a source and a sink of greenhouse gas.

To get a full understanding of these dynamics, two locations in the anoxic zone should be monitored continuously. To understand the net effect of this zone in terms of emissions risk, a single measurement location at the end of the zone is ideal, as here the water passes back to the aeration where stripping takes place.

Conclusion

In summary, this research has shown that with two liquid phase sensors, the process dynamics and emission patterns in some of the most common reactor types can be determined in an accurate and representative way. The same has previously been shown for another set of carousel reactors². For plug flow reactors, which often exhibit shift of nitrification points over time, more scouting may be needed for positioning of N₂O sensors³.

To determine the emissions, a reliable measurement of the airflow is also necessary. To provide the most trustworthy value, this is ideally taken from a flow meter in the pipe that delivers air to the aerated zone. If air flows are measured with a floating hood at the surface of the reactor instead, an inhomogeneous distribution of air must be assumed. The floating hood must therefore be moved to various locations for long enough to measure a representative sample.

Authors: Floris de Heer, IMD & Dr. Bastian Piltz, Unisense Environment

Literature

¹ Unisense Environment, 2024. "N₂O Mass Transfer Coefficient Calculation from Aeration Field Size and Air Flow", <https://unisense-environment.com/manuals/>

² Unisense Environment, 2021. "Positioning of the N₂O wastewater sensor", <https://unisense-environment.com/applications/positioning-of-n2o-wastewater-sensor/>

³ Unisense Environment, 2023. "N₂O Monitoring Highlights Potential for GHG Emissions Reductions", <https://unisense-environment.com/applications/n2o-monitoring-highlights-potential-for-ghg-emissions-reduction/>

Version: November 2024

UNISENSE 
ENVIRONMENT 

Nitrous Oxide process sensor for online
wastewater treatment optimization,
low-cost greenhouse gas reduction,
and reliable sustainability accounting

Unisense Environment A/S

Web: www.unisense-environment.com

LinkedIn: [Unisense Environment](https://www.linkedin.com/company/unisense-environment)

E-mail: sales@unisense.com

Phone: +45 8944 9500

Office hours:

Monday–Thursday 8 am to 4 pm (CET)

Friday 8 am to 3.30 pm (CET)

measure
to kN₂O_w

